## Globe valve

(MILLER)


## Model description:

This model of component calculates the minor head loss (pressure drop) generated by the flow in a globe valve installed in a straight pipe.

## Model formulation:

Cross-sectional area at valve inlet ( $m^{2}$ ):
$\mathrm{A}=\pi \cdot \frac{D^{2}}{4}$

Mean velocity ( $\mathrm{m} / \mathrm{s}$ ):

$$
U=\frac{Q}{A}
$$

Mass flow rate ( $\mathrm{kg} / \mathrm{s}$ ):

$$
G=Q \cdot \rho
$$

Reynolds number:

$$
\operatorname{Re}=\frac{U \cdot D}{v}
$$

Local resistance coefficient:

- $R e \geq 10^{4}$ (turbulent flow)

$$
K_{\text {turb }}=f(\alpha)
$$



- $\operatorname{Re}<10^{4}$ (laminar flow)

$$
K_{\text {lam }}=f\left(K_{\text {turb }}, \mathrm{Re}\right)
$$

([1] figure 14.31)

Laminar loss coefficient relationship to turbulent loss coefficient MILLER - Figure 14.31 ( $\mathrm{Re}<1 \mathrm{e} 4$ )


Reynolds Number Correction ( $\operatorname{Re}<10^{4}$ ):

$$
C_{\mathrm{Re}}=\frac{K_{\text {lam }}}{K_{\text {turb }}}
$$

Total pressure loss coefficient (based on mean velocity):

- turbulent flow ( $\operatorname{Re} \geq 10^{4}$ ):

$$
K=K_{\text {turb }}
$$

- laminar flow ( $\mathrm{Re}<10^{4}$ ):
$K=K_{\text {lam }}$

Total pressure loss ( Pa ):
$\Delta P=K \cdot \frac{\rho \cdot U^{2}}{2}$

Total head loss of fluid (m):
$\Delta H=K \cdot \frac{U^{2}}{2 \cdot g}$

Hydraulic power loss (W):

$$
W h=\Delta P \cdot Q
$$

Symbols, Definitions, SI Units:
$D \quad$ Internal diameter ( $m$ )
A Cross-sectional area ( $\mathrm{m}^{2}$ )
Q Volume flow rate ( $\mathrm{m}^{3} / \mathrm{s}$ )
$G \quad$ Mass flow rate (kg/s)
$U \quad$ Mean velocity ( $\mathrm{m} / \mathrm{s}$ )
Re Reynolds number ()
st Opening stroke of the valve (\%)
Kturb Local resistance coefficient for $\operatorname{Re} \geq 10^{4}$ ()
Klam Local resistance coefficient for $\operatorname{Re}<10^{4}$ ()
$C_{\operatorname{Re}} \quad$ Reynolds number correction for $\mathrm{Re}<10^{4}$ ()
$K \quad$ Total pressure loss coefficient (based on mean velocity) ()
$\Delta \mathrm{P} \quad$ Total pressure loss ( Pa )
$\Delta H \quad$ Total head loss of fluid (m)
Wh Hydraulic power loss (W)
$\rho \quad$ Fluid density $\left(\mathrm{kg} / \mathrm{m}^{3}\right)$
$v \quad$ Fluid kinematic viscosity ( $\mathrm{m}^{2} / \mathrm{s}$ )
$9 \quad$ Gravitational acceleration $\left(\mathrm{m} / \mathrm{s}^{2}\right)$

## Validity range:

- any flow regime: laminar and turbulent
note: for laminar flow regime $\left(\operatorname{Re}<10^{4}\right)$, the pressure loss coefficient "Klam" is estimated

Example of application:
Fluid characteristics
Fluid: $\quad$ Water @ $1 \mathrm{~atm}[\mathrm{HC}]$

Ref.: IAPWS IF97

Ref.: IAPWS IF97


Pressure:

| Density: | $\rho$ | 998.2061 | $\mathrm{~kg} / \mathrm{m}^{3}$ |
| :--- | :--- | ---: | :--- |
| Dynamic Viscosity: | $\mu$ | 0.00100159 | $\mathrm{~N} . \mathrm{s} / \mathrm{m}^{2}$ |
| Kinematic Viscosity: | v | $1.00340 \mathrm{E}-06$ | $\mathrm{~m}^{2} / \mathrm{s}$ |

( Density $\bigcirc$ Dyn. Visc. Kin. Visc.


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Complementary results

| Designation | Symbol | Value | Unit |
| :---: | :---: | :---: | :---: |
| Pipe cross-section area | A | 0.003881508 | $\mathrm{m}^{2}$ |
| Reynolds number | Re | 90251 |  |
| Coefficient of local resistance (Figure 14.24) | Kturb | 3.9632 |  |
| Pressure loss coefficient (based on the mean valve velocity) | K | 3.9632 |  |
| Hydraulic power loss | Wh | 16.41138 | w |
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## References:

[1] Internal Flow System, Second Edition, D.S. Miller

## HydrauCalc

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