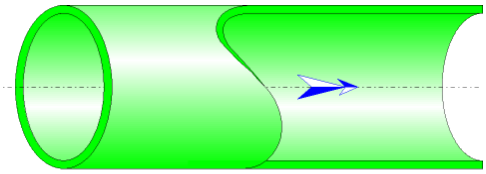
Straight Pipe
Circular Cross-Section and Roughness Walls
(MILLER)



Model description:

This model of component calculates the major head loss (pressure drop) of a horizontal straight pipe of circular and constant cross-section.
In addition, the flow is assumed fully developed and stabilized.

The head loss is due to the friction of the fluid on the inner walls of the piping and is calculated with the Darcy formula.

Darcy friction factor is determined:

- for laminar flow regime by the law of Hagen-Poiseuille (independent of the value of relative roughness),
- for turbulent flow regime by the explicit Swamee-Jain equation (dependent of the value of relative roughness), the explicit Swamee-Jain equation is a Colebrook-White equation approximation,
- for critical flow regime by interpolation between friction factors of laminar and turbulent flow.

Model formulation:

Hydraulic diameter (m):

$$\boxed{D = d}$$

Cross-section area (m²):

$$\boxed{A = \pi \cdot \frac{d^2}{4}}$$

Mean velocity (m/s):

$$\boxed{U = \frac{Q}{A}}$$

Mass flow rate (kg/s):

$$m = Q \cdot \rho$$

Fluid volume in the pipe (m^3):

$$V = A \cdot L$$

Fluid mass in the pipe (kg):

$$M = V \cdot \rho$$

Reynolds number:

$$\mathrm{Re} = \frac{U \cdot D}{\nu}$$

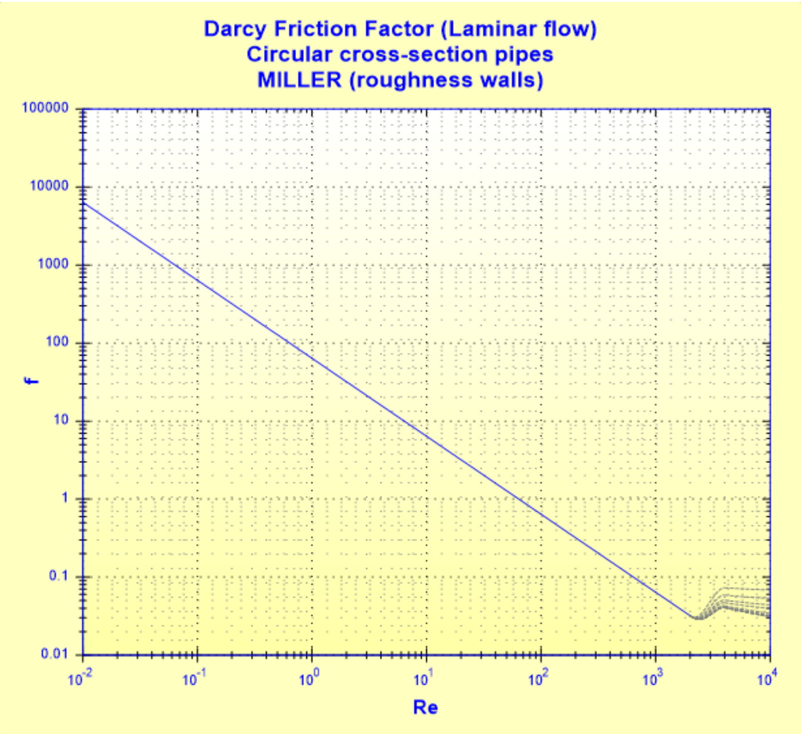
Darcy friction factor:

- laminar flow regime (Re ≤ 2000):

  Hagen-Poiseuille law

$$f = \frac{64}{\mathrm{Re}}$$

([1] equation 8.7)



- turbulent flow regime – transition region and complete turbulence region (Re ≥ 4000):

  Swamee-Jain equation (Colebrook-White equation approximation)

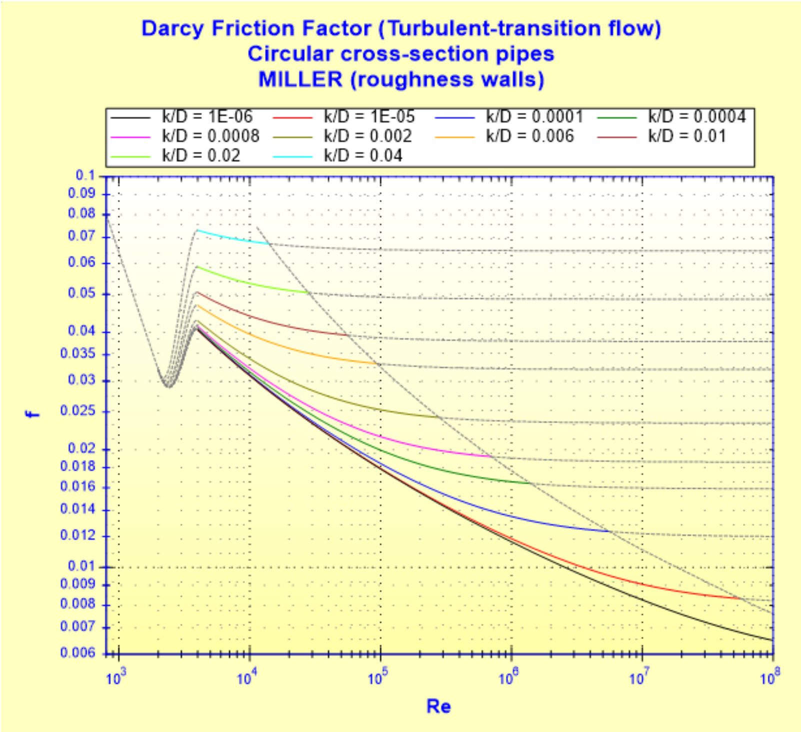
$$f = \frac{0.25}{\left[\log\left(\frac{k}{3.7 \cdot D} + \frac{5.74}{\mathrm{Re}^{0.9}}\right)\right]^2}$$

([1] equation 8.4)

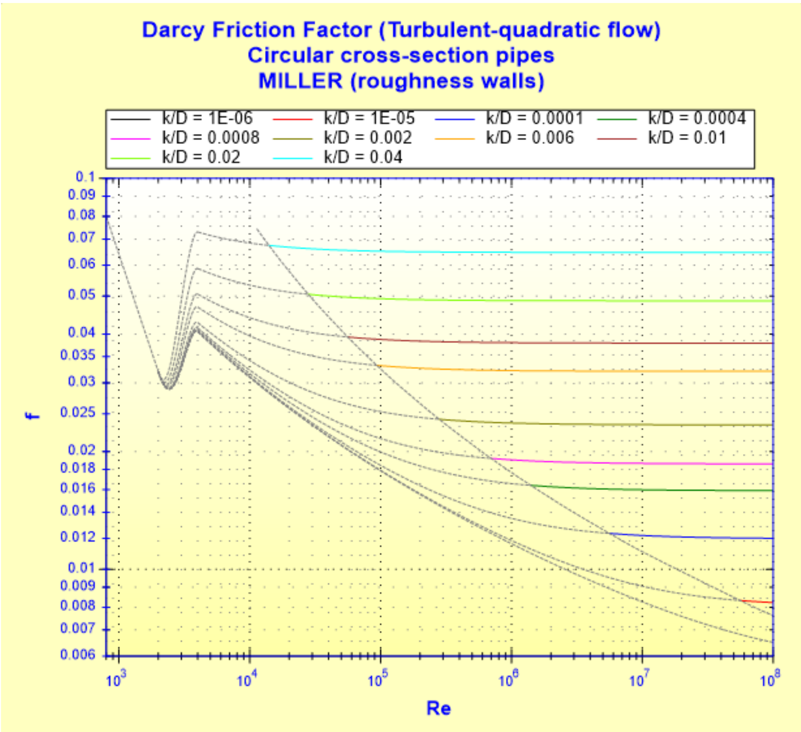
Reynolds number corresponding to the beginning of complete turbulence:

$$\boxed{Re''_{lim} = \frac{560}{\overline{\Delta}}}$$ ([2] diagram 2.4)

Transition region



Complete turbulence region



- critical flow regime (2000 < Re < 4000):

  cubic interpolation

  $$\boxed{f = (X1 + R \cdot (X2 + R \cdot (X3 + X4)))}$$ ([3])

  with:

$$R = \frac{Re}{2000}$$

$$X1 = 7 \cdot FA - FB$$

$$X2 = 0.128 - 17 \cdot FA + 2.5 \cdot FB$$

$$X3 = -0.128 + 13 \cdot FA - 2 \cdot FB$$

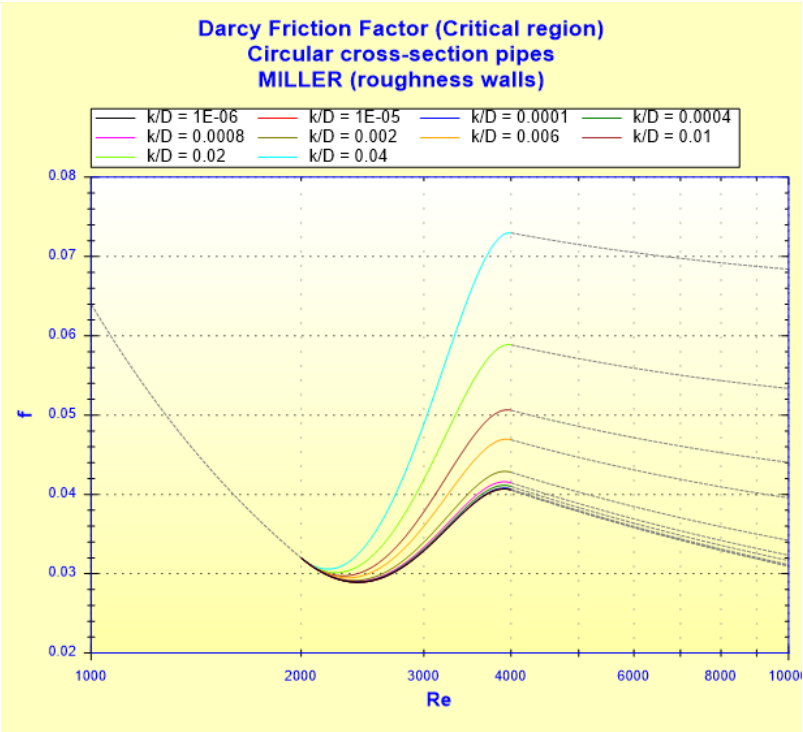
$$X4 = R \cdot (0.032 - 3 \cdot FA + 0.5 \cdot FB)$$

$$FA = Y3^{-2}$$

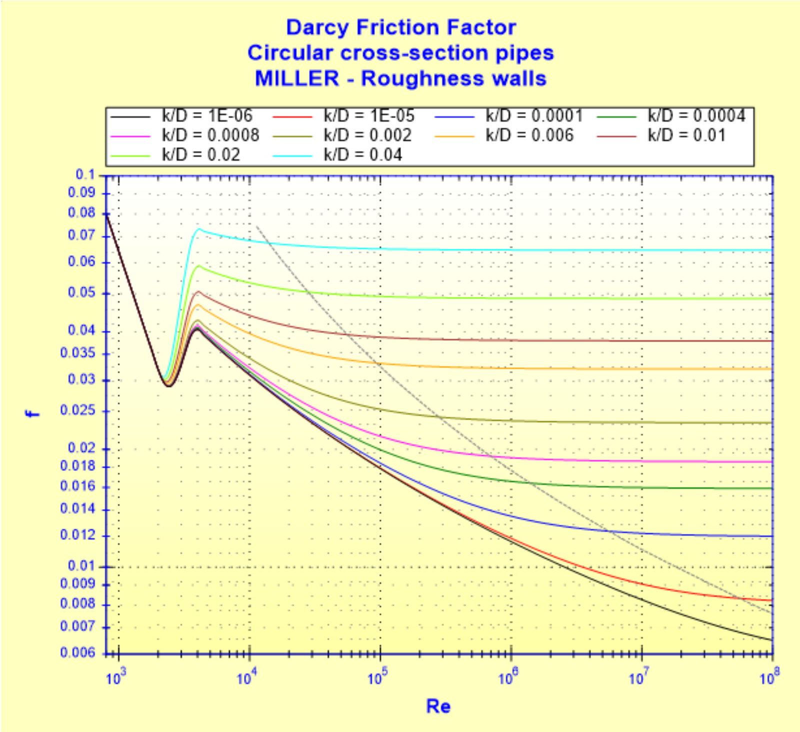
$$FB = FA \cdot \left(2 - \frac{0.00514215}{Y2 \cdot Y3}\right)$$

$$Y2 = \frac{k}{3.7 \cdot D} + \frac{5.74}{Re^{0.9}}$$

$$Y3 = -0.86859 \cdot ln\left(\frac{k}{3.7 \cdot D} + \frac{5.74}{4000^{0.9}}\right)$$



■ all flow regimes:



Friction pressure loss coefficient:

$$K_f = f \cdot \frac{L}{D}$$

([1] equation 8.3)

Total pressure loss coefficient (based on the mean pipe velocity):

$$K = K_f$$

Total pressure loss (Pa):

$$\Delta P = K \cdot \frac{\rho \cdot U^2}{2}$$

([1] equation 8.1b)

Total head loss of fluid (m):

$$\Delta H = K \cdot \frac{U^2}{2 \cdot g}$$

([1] equation 8.1a)

Hydraulic power loss (W):

$$Wh = \Delta P \cdot Q$$

Symbols, Definitions, SI Units:

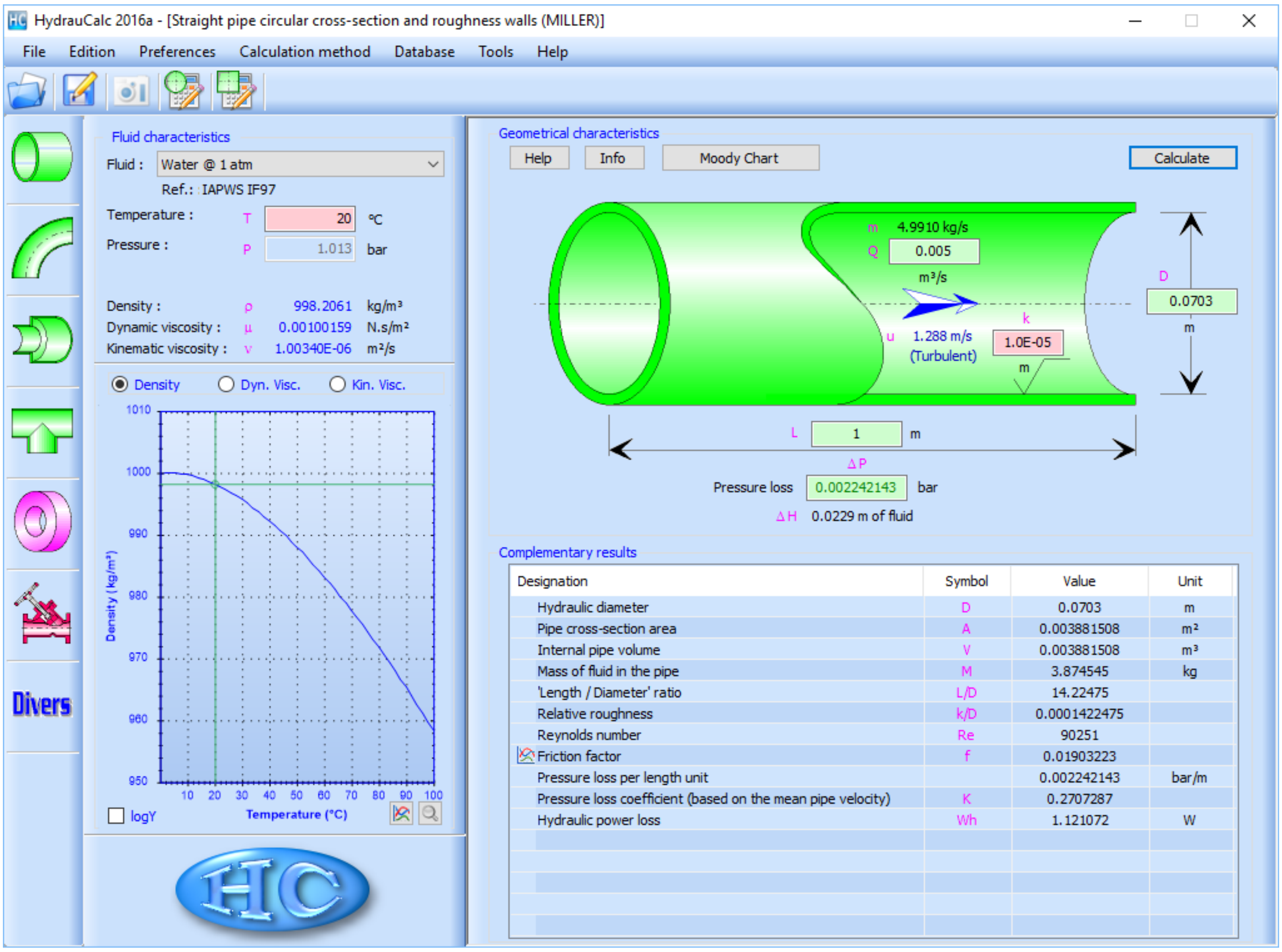
D	Hydraulic diameter (m)
d	Internal diameter (m)
A	Cross-section area (m^2)
Q	Volume flow rate (m^3/s)
m	Mass flow rate (kg/s)
U	Mean velocity (m/s)
L	Pipe length (m)
V	Fluid volume in the pipe (m^3)

M	Fluid mass in the pipe (kg)
Re	Reynolds number ()
Re''_{lim}	Nombre de Reynolds correspondant au début de la turbulence complète ()
k	Absolute roughness of walls (m)
f	Darcy friction factor ()
K_f	Friction pressure loss coefficient ()
K	Total pressure loss coefficient (based on the mean pipe velocity) ()
ΔP	Total pressure loss (Pa)
ΔH	Total head loss of fluid (m)
Wh	Hydraulic power loss (W)
ρ	Fluid density (kg/m^3)
ν	Fluid kinematic viscosity (m^2/s)
g	Gravitational acceleration (m/s^2)

Validity range:

- any flow regime: laminar, critical and turbulent ($Re \leq 10^8$)
- $k/D \leq 0.05$
- stabilized flow

Example of application:



References:

[1] Internal Flow System, Second Edition, D.S. Miller (1990)
[2] Handbook of Hydraulic Resistance, 3rd Edition, I.E. Idelchik (2008)
[3] Dunlop (1991)

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