## Straight Pipe <br> Circular Cross-Section and Uniform Roughness Walls (IDELCHIK)



## Model description:

This model of component calculates the major head loss (pressure drop) of a horizontal straight pipe of circular and constant cross-section.
In addition, the flow is assumed fully developed and stabilized.

The head loss is due to the friction of the fluid on the inner walls of the piping and is calculated with the Darcy formula. The roughness of the inner walls of the pipe is supposed uniform (pipe used by Nikuradse for its experimental data).

Darcy friction factor is determined:

- for laminar flow regime by the law of Hagen-Poiseuille (independent of the value of relative roughness),
- for turbulent flow regime by the Nikuradse equation (dependent of the value of relative roughness),
- for critical flow regime by interpolation between friction factors of laminar and turbulent flow.


## Model formulation:

Hydraulic diameter (m):

$$
\mathrm{D}_{\mathrm{h}}=D_{0}
$$

Cross-section area ( $m^{2}$ ):
$\mathrm{F}_{0}=\pi \cdot \frac{D_{0}{ }^{2}}{4}$

Mean velocity ( $\mathrm{m} / \mathrm{s}$ ):

$$
w_{0}=\frac{Q}{F_{0}}
$$

Fluid volume in the pipe $\left(m^{3}\right)$ :

$$
\mathrm{V}=F_{0} \cdot 1
$$

Fluid mass in the pipe (kg):

$$
\mathrm{M}=V \cdot \rho
$$

Reynolds number:

$$
\mathrm{Re}=\frac{w_{0} \cdot D_{h}}{v}
$$

Relative roughness:
$\bar{\Delta}=\frac{\Delta}{D_{h}}$

Darcy friction factor:

- laminar flow regime ( $\mathrm{Re} \leq 2000$ ):

Hagen-Poiseuille law

$$
\lambda=\frac{64}{\mathrm{Re}}
$$

([1] diagram 2.1)


- turbulent flow regime - transition region and complete turbulence region ( $\mathrm{Re} \geq$ 4000):

Nikuradze equation

$$
\lambda=\frac{1}{\left[a_{1}+b_{1} \cdot \log (\operatorname{Re} \cdot \sqrt{\lambda})+c_{1} \cdot \log (\bar{\Delta})\right]^{2}}
$$

where the values of $a_{1}, b_{1}$ and $c_{1}$ are given below:

| $\bar{\Delta} \cdot \operatorname{Re} \cdot \sqrt{\lambda}$ | $\mathrm{a}_{1}$ | $\mathrm{~b}_{1}$ | $\mathrm{c}_{1}$ |
| :---: | :---: | :---: | :---: |
| $3.6-10$ | -0.800 | 2.000 | 0.000 |
| $10-20$ | 0.068 | 1.130 | -0.870 |
| $20-40$ | 1.538 | 0.000 | -2.000 |
| $40-191.2$ | 2.471 | -0.588 | -2.588 |
| $>191.2$ | 1.138 | 0.000 | -2.000 |

Reynolds number at which pipe cease to be hydraulically smooth:
$\operatorname{Re}^{\prime}{ }_{\text {lim }}=\frac{26.9}{\Delta^{-1.143}}$
Reynolds number corresponding to the beginning of complete turbulence:
$R{ }^{\prime \prime}{ }_{\text {lim }}=\frac{217.6-382.4 \cdot \log (\bar{\Delta})}{\bar{\Delta}}$
([1] diagram 2.2)

## Transition region



Complete turbulence region


■ critical flow regime (2000 < Re < 4000):
linear interpolation
$\lambda=\lambda_{L} \cdot\left(1-\frac{R e-2000}{2000}\right)+\lambda_{T} \cdot\left(\frac{R e-2000}{2000}\right)$
with:
$\lambda_{L}=$ laminar friction coefficient obtained with $R e=2000$
$\lambda_{T}=$ turbulent friction coefficient obtained with $R e=4000$


- all flow regimes:


Pressure loss coefficient (based on the mean pipe velocity):
$\zeta=\lambda \cdot \frac{l}{D_{h}}$
([1] equation 2-2)

Total pressure loss (Pa):

$$
\Delta P=\zeta \cdot \frac{\rho \cdot w_{0}^{2}}{2}
$$

([1] equation 2-2)

Total head loss of fluid (m):

$$
\Delta H=\zeta \cdot \frac{w_{0}^{2}}{2 \cdot g}
$$

Hydraulic power loss (W):

$$
W h=\Delta P \cdot Q
$$

## Symbols, Definitions, SI Units:

Dh Hydraulic diameter ( $m$ )
Do Internal diameter ( $m$ )
Fo Cross-sectional area ( $\mathrm{m}^{2}$ )
Q Volume flow rate ( $\mathrm{m}^{3} / \mathrm{s}$ )
$G \quad$ Mass flow rate ( $\mathrm{kg} / \mathrm{s}$ )
wo Mean velocity ( $\mathrm{m} / \mathrm{s}$ )
$1 \quad$ Pipe length ( $m$ )
$V \quad$ Fluid volume in the pipe $\left(m^{3}\right)$
$M \quad$ Fluid mass in the pipe ( kg )
Re Reynolds number ()
Re'lim Limiting Reynolds number for hydraulically smooth law ()

Re"lim Limiting Reynolds number for quadratic law ()
$\Delta \quad$ Absolute roughness of walls ( $m$ )
$\bar{\Delta} \quad$ Relative roughness of walls ()
$\lambda \quad$ Darcy friction factor ()
$\zeta \quad$ Pressure loss coefficient (based on the mean pipe velocity) ()
$\Delta \mathrm{P} \quad$ Total pressure loss ( Pa )
$\Delta H \quad$ Total head loss of fluid (m)
Wh Hydraulic power loss (W)
$\rho \quad$ Fluid density $\left(\mathrm{kg} / \mathrm{m}^{3}\right)$
$v \quad$ Fluid kinematic viscosity ( $\mathrm{m}^{2} / \mathrm{s}$ )
$9 \quad$ Gravitational acceleration $\left(\mathrm{m} / \mathrm{s}^{2}\right)$

## Validity range:

- any flow regime: laminar, critical and turbulent $\left(\operatorname{Re} \leq 10^{8}\right)$
- $\bar{\Delta} \leq 0.05$
- stabilized flow


## Example of application:



## References:

[1] Handbook of Hydraulic Resistance, 3rd Edition, I.E. Idelchik (2008)

HydrauCalc
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